



Alternative Ways to Achieve Class A Biosolids

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6th Waste Treatment Symposium


What will be discussed?


- **Waste Characteristics & Disinfection**
- **Individual & Collective Treatment**
- **40CFR503 - Class A Alternative Treatment Methods**
- **Examples of Ways to Achieve Class A**





Characteristics of Septage

Parameter	Concentration	
	Minimum	Maximum
Total solids	1,132	130,475
Total volatile solids	353	71,402
Total suspended solids	310	93,378
Volatile suspended solids	95	51,500
Biochemical oxygen demand	440	78,600
Chemical oxygen demand	1,500	703,000
Total Kjeldahl nitrogen	66	1,060
Ammonia nitrogen	3	116
Total phosphorus	20	760
Alkalinity	522	4,190
Grease	208	23,368
pH	1.5	12.6
Total coliform	10 ⁷ /100 mL	10 ⁹ /100 mL
Fecal coliform	10 ⁷ /100 mL	10 ⁹ /100 mL



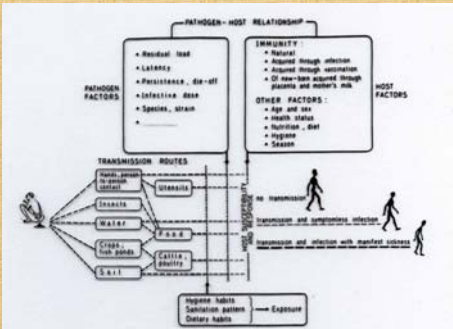
SOURCES OF WASTEWATER & ASSOCIATED MICROORGANISMS











ROUTES OF INFECTION






CONCERNS / ISSUES



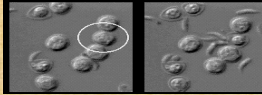


Some culprits...


Giardia Lamblia



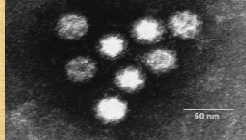
Cryptosporidium parvum




E.coli



Calicivirus




... What are others?




Pathogens Potentially Present

PATHOGEN CLASS	EXAMPLES	DISEASE
Bacteria	<i>Shigella sp.</i>	Bacillary dysentery
	<i>Salmonella sp.</i> <i>Salmonella typhi</i> <i>Vibrio cholerae</i>	Salmonellosis (gastroenteritis) Typhoid fever Cholera
Viruses	Enteropathogenic- <i>Escherichia coli</i>	A variety of gastroenteric diseases
	<i>Yersinia sp.</i>	Yersiniosis (gastroenteritis)
	<i>Campylobacter jejuni</i>	Campylobacteriosis (gastroenteritis)
Viruses	Hepatitis A	Infectious hepatitis
	Norwalk virus	Acute gastroenteritis
	Rotaviruses	Acute gastroenteritis
	Polioviruses	Polio myelitis
	Coxsackie viruses	"flu-like" symptoms
Echoviruses	"flu-like" symptoms	




Pathogens Potentially Present Continued

PATHOGEN CLASS	EXAMPLES	DISEASE
Protozoa	<i>Entamoeba histolytica</i>	Amebiasis (amoebic dysentery)
	<i>Giardia lamblia</i>	Giardiasis (gastroenteritis)
	<i>Cryptosporidium sp.</i>	Cryptosporidiosis (gastroenteritis)
	<i>Balantidium coli</i>	Balantidiasis (gastroenteritis)
Helminths	<i>Ascaris sp.</i>	Ascariasis (roundworm infection)
	<i>Taenia sp.</i>	Taeniasis (tapeworm infection)
	<i>Necator americanus</i>	Ancylostomiasis (hookworm infection)
	<i>Trichuris trichuria</i>	Trichuriasis (whipworm infection)



Indicator and Pathogen Organism Concentrations in Domestic Septage



Parameter	Typical Range (counts/100 ml)	Reference
Total Coliform	10 ⁷ - 10 ⁹	(10)
Fecal Coliform	10 ⁶ - 10 ⁸	(9) (10) (23)
Fecal Streptococci	10 ⁶ - 10 ⁷	(9) (10) (23)
Ps. Aeruginosa	10 ¹ - 10 ³	(9) (10) (23)
Salmonella Sp.	1 - 10 ²	(9) (10)
Parasites		
Toxocara, Ascaris Lumbricoides, Trichuris Trichura, Trichuris Vulpis	Present	(10)



Dose Response Data Viruses and Parasites

ORGANISM	INFECTIVE DOSE
Poliovirus	1 TCID50, < 1PFU
Cryptosporidium	10 cysts
Giardia lamblia	1 cyst
Helminths	1 egg



All above infective doses are estimates.

Using Multiple Barriers to Protect The Public Health

- **Disinfection**
- **Stabilization (Vector Attraction Control)**
- **Cropping and Access Restrictions**
- **Storage**

Approach taken by US.

Some Disinfection History

2000 BC

Roman Times

Heavy Metals - Cu

FACTORS ILLUSTRATED
 Solar Radiation
 Drying / Desiccation
 Heat & Time
 pH
 Filtration
 Heavy Metals
 Storage / Stabilization

Standard Treatment Procedure for achieving disinfection and vector attraction control – Using Lime

Add lime to residential septage to raise pH to 12.0

Uses approximately 15, 000 mg/L of lime

Beneficially use

SEPTAGE RECEIVING STATION & TREATMENT SYSTEM

Earth Berm w/ "Green Belt" Plantings & Screenings

In

Decant Holding Tank

Solid PreCast Plank Top Panels

Isolation Valve

Carbon Canister for Odor Control

2 Compartment Storage Tank

Liquid Lime Holding Tank w/ B-2 Liquid Lime PLC Panel

Lime Stabilization Tank w/ Mixer

Key Card Reader

Out

Loading Station for Trucking Decant to WWTP or Stabilized BioSolids to Land Application Site

Floor Sloped to Pump

Septage Receiving Station Screens w/ Dumpster for Screenings

Septage Truck

Note: Standard Tank Design is for Backfill to Top of Tank. Optional FreeStanding Design is Available

Typical Community Management of Septage and WWTP Residuals

Individual Onsite Systems

- land application
- surface (land) disposal
- incineration

Sewer Area

- consultation with wastewater treatment facility
- land application of biosolids
 - agricultural and industrial use
 - landfills
 - land treatment
 - landfills
 - landfills
 - landfills

land application of biosolids

- agricultural and industrial use
- landfills
- land treatment
- landfills
- landfills
- landfills

Class A Sludge Microbiological Criteria

- Must be met by all Alternatives
 - Salmonella = < 3 MPN per 4 g of TS OR
 - Fecal Coliforms = < 1000 MPN per gram of TS
- Must use PFRP Process or Show
 - Enteric Viruses = < 1 PFU per 4 g of TS AND
 - Viable Helminth Ova = < 1 per 4 g of TS

SIX CLASS A ALTERNATIVES

1. Meet time-temperature requirement – 19%
2. pH > 12 and temp. > 52°C for 12 h. – 12%
3. Measure V.H. eggs and enterovirus before and after process. If none after process and enough tests, you are O.K. – 4%
4. Test each batch for VHE and enterovirus – 9%
5. Use a PFRP – 52%
6. Use a PFRP- Equivalent - ~ 2-3%

Time and Temperature Guidelines

Total Solids	Temp. (°C)	Time (D)	Equation	Notes
≥7%	≥50°C	≥20 min.	$D = \frac{111,700,000}{10^{(T-50)}}$	No heating of small particles by warmed gases or immiscible liquid.
≥7%	≥50°C	≥15 sec.	$D = \frac{111,700,000}{10^{(T-50)}}$	Small particles heated by warmed gases or immiscible liquid.
<7%	>50°C	≥15 sec. to <30 min.	$D = \frac{111,700,000}{10^{(T-50)}}$	
<7%	≥50°C	≥30 min.	$D = \frac{50,070,000}{10^{(T-50)}}$	

* in no case would temperatures calculated using the appropriate equation be less than 50°C



Time / Temperature Relationships for Class A Pathogen Reduction



THERMAL PROCESSES USING EQUATIONS TO ACHIEVE CLASS A

- THERMOPHILIC ANAEROBIC DIGESTION
- THERMOPHILIC AEROBIC DIGESTION
- PASTEURIZATION
- HEAT DRYING
- OTHER



BATCH



Alternative 2: Sewage Sludge Treated in a High pH-High Temperature Process (Alkaline Treatment) [503.32(a)(4)]

This alternative describes conditions of a high temperature-high pH process that has proven effective in reducing pathogens to below detectable levels. The process conditions required by the Part 503 regulation are: Elevating pH to greater than 12 and maintaining the pH for more than 72 hours.

Maintaining the temperature above 52°C (126°F) throughout the sewage sludge for at least 12 hours during the period that the pH is greater than 12.

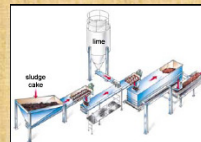
Air drying to over 50% solids after the 72-hour period of elevated pH.

The hostile conditions of high pH, high temperature, and reduced moisture for prolonged time periods allow a variance to a less stringent time-temperature regime than for the thermal requirements under Alternative 1. The pH of the sewage sludge is measured at 25°C (77°F) or an appropriate correction is applied.





Class A: Alternative 5 – PFRP Processes

PFRP	
Composting	Be maintained at 55°C or greater for 3 d using in-vessel or static aerated pile composting OR for 15 d, during which compost is turned at least 5 times, in windrows.
Heat Drying	Be dried to 10% moisture or lower AND reach more than 80°C.
Heat Treatment	Be maintained at 180°C for 30 min.
Thermophilic Aerobic Digestion	Be maintained at 55-60°C for 10 d (hydraulic residence time). Volatile solids content must also be reduced at least 38%.
PFRP + Beta Ray Irradiation	Be irradiated with beta rays from an accelerator at dosages of at least 1.0 megarad at room temperature.
PFRP + Gamma Ray Irradiation	Same as above except irradiation is with gamma rays from isotopes like cobalt or cesium.
PFRP + Pasteurization	Be maintained at 70°C for at least 30 min.



ALT. 6: PFRP EQUIVALENT PROCESSES (4 %)

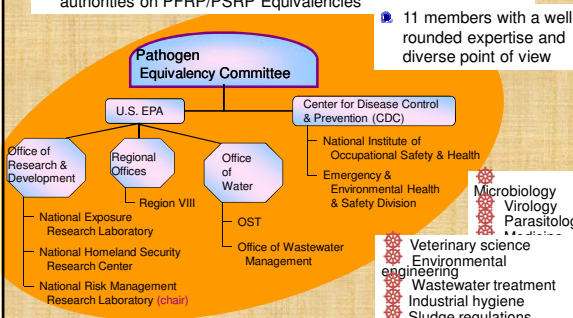
- BIOSET
- Biochem - BCR
- J vap - US Filter
- Thermophilic Anaerobic Digestion
 - Columbus, Georgia
 - EBMUD
 - Lyonnaise des Eaux - Infilco Degremont
 - Los Angeles
- ATAD
- Magnagro


Pathogen Equivalency Committee

Created in 1985 to provide technical expertise to permitting authorities on PFRP/PSRP Equivalencies


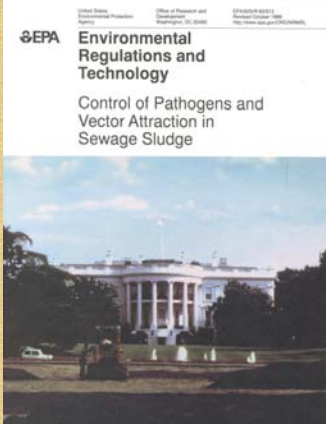
11 members with a well-rounded expertise and diverse point of view





www.epa.gov/nrmrl/pec/index.html



Criteria for Demonstrating Disinfection Equivalency		
Mandatory Minimum Requirements		
	PSRP Equivalency	PFRP Equivalency
Process Efficiency Parameters:	≥ 2 log reduction of fecal coliform bacteria	1) ≥ 3 log reduction of total enteric viruses, and
	and/or	2) ≥ 2 log reduction of viable helminth (<i>Ascaris</i>) ova, and
	≥ 2 log reduction of <i>E. coli</i> bacteria	3) ≥ 5 log reduction of fecal coliform bacteria
	and/or	
	≥ 2 log reduction of <i>Enterococcus</i> spp. bacteria	and/or
	and/or	≥ 5 log reduction of <i>E. coli</i> bacteria
Process Compliance Parameters (The 40CFR503 Requirements):	2,000,000 MPN or CFU/g total Solids (TS) of fecal coliform in the treated sludge	Organism densities in the treated sludge of:
		1) ≤ 1 pfu/4 g TS of total enteric viruses, and
		2) ≤ 3 viable helminth (<i>Ascaris</i>) ova/4 g TS, and
		3) ≤ 1,000 MPN fecal coliform / g TS or = 3 MPN <i>Salmonella</i> spp./4 g
		and/or
		≥ 4 log reduction of <i>Salmonella</i> spp. bacteria
	and/or	≥ 4 log reduction of somatic bacteriophages

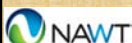



EPA Environmental Regulations and Technology
Control of Pathogens and Vector Attraction in Sewage Sludge

- The sludge is held at a temperature of 55°C or greater for a minimum of 25 minutes.
- The solids content of the sludge being treated is in the range of 6% to 35%.
- The ammonia content in the reactor is 1% (10,000 mg/L) on a volume basis.
- The pressure in the reactor is 30 psi.
- The amount of lime added is 0.55 to 0.75 lbs. lime to 1 dry lb. of sludge.
- The amount of sulfamic acid added is 8 to 10 lbs. per dry ton of sludge.
- The pH is greater than 12.


From USEPA-DW-Approval letter of Equivalency

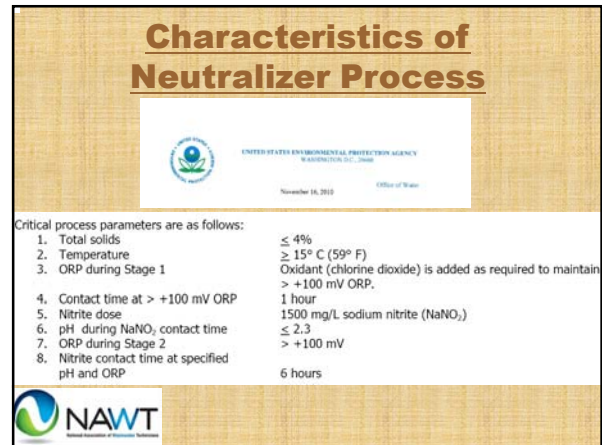
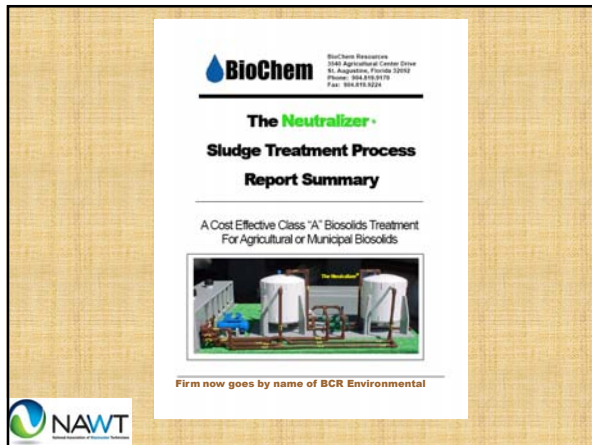
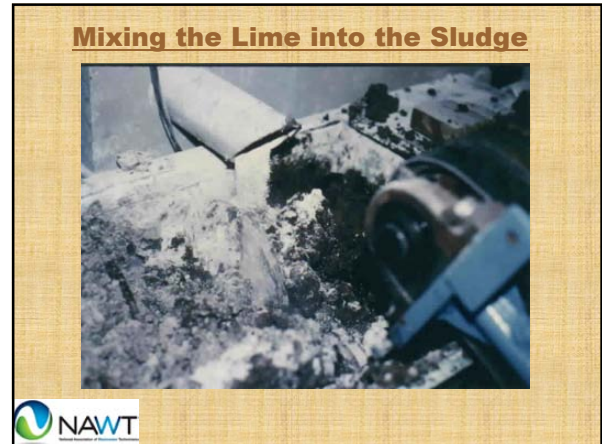


Influence of Temperature, Time, % Ammonia, & Pressure on *Ascaris* Inactivation

LOCATION	DATE	RUN #	TEMP	TIME IN UNIT	% REDUCTION OF <i>Ascaris</i>	% AMMONIA	PRESSURE KPa (psi)
Morgan City	28-May-02	1	42°C	85 min	97.4	0.5	103 (15)
	30-May-02	2	50°C	104 min	87.5	0.05	103 (15)
Kingwood	4-Jun-02	1	45°C	25 min	69.9	0.5	207 (30)
	6-Jun-02	2	46°C	25 min	89.7	0.9	207 (30)
	7-Jun-02	3	55°C	25 min	100	1.0	207 (30)
Sulphur	8-Jul-02	1	50°C	14 min	98.6	0.7*	262 (38)
	9-Jul-02	2	55°C	11 min	100	0.8*	262 (38)

* Estimated values based on previous research


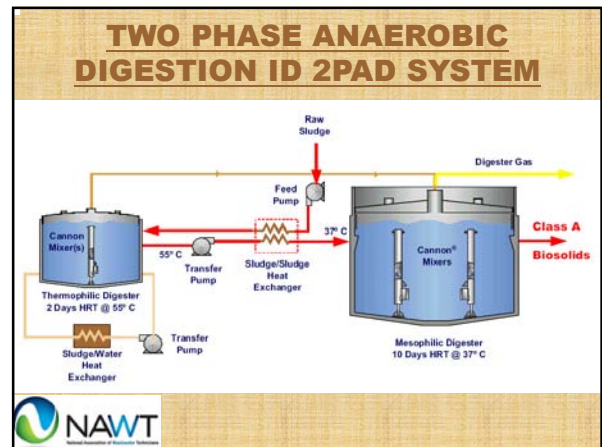




Disinfection Capability of Neutralizer Process

Pathogen	Spike Concentration (per 4 g DWS*)	Recovered from Controls (per 4 g DWS)	Recovered after Treatment (per 4 g DWS)	Log Reduction
<i>Ascaris</i> eggs	5 x 10 ⁴	4.5 x 10 ⁴	< 1	4
Poliovirus	1.1 x 10 ⁵	3.5 x 10 ⁴	< 1	4
	Raw Concentration (MPN/g)	Recovered from Controls (MPN/g)**	Recovered after Treatment (MPN/g)	Log Reduction
Fecal Coliform***	2 x 10 ⁹	2 x 10 ⁹	< 1	9

*Dry weight solids **Most probable number per gram dry weight ***Fecal coliform results are from tests conducted on raw sludge.





Lyonnais des Eaux's Two-Phase Thermo-Meso Feed Sequencing Anaerobic Digestion Process

Sewage sludge is treated in the absence of air in an acidogenic thermophilic reactor and a mesophilic methanogenic reactor connected in series. The mean cell residence time shall be at least 2.1 days (± 0.05 d) in the acidogenic thermophilic reactor followed by 10.5 days (± 0.3 d) in the mesophilic methanogenic reactor.

Feeding of each digester shall be intermittent and occurring 4 times per day every 6 hours. The mesophilic methanogenic reactor shall be fed in priority from the acidogenic thermophilic reactor.


Between two consecutive feedings temperature inside the acidogenic thermophilic reactor should be between 49 C and 55 C with 55 C maintained during at least 2.8 hours. Temperature inside the mesophilic methanogenic reactor shall be constant and at least 37 C.

 *Run like a batch process – nothing entering or leaving.*

Performance of 2PAD System Pilot Plant


Variable	Feed Sludge	Acidogenic Digester	Methanogenic Digester
	Mean	Mean	Mean
# Feedings per day	-	4	4
Temperature (°C)	-	55 - 56	37
pH	5.57	6.0	7.2
TS (g/L)	38.5	27.8	21.2
VS (g/L)	27.8	21.3	12.1
VSR	-	23.8	40
VFA total (mgHAc/L)	1,393.3	2,309.8	203
Total ammonia (mg/L)	47.7	552	763.5
Fecal coliform Log (MPN/gTS)	> 6.35	0.9	0.38
Enterovirus Log(PFU/4g TS)	4.04	BD	BD
Viable <i>ascaris</i> eggs Log (count/4gTS)	2.61	BD	BD

All pathogen densities are shown in log₁₀. TS: Total Solids, VS: Volatile Solids, TSS: Total Suspended Solids, VSS: Volatile Suspended Solids, BD: Below Detection, HAc: Acetic acid, VFA: Volatile Fatty Acids, VSR: Volatile Solids Reduction



Some Additional Examples of Ways to Attain Class A that may be useful to Small Facilities

- **Quick Lime Processes**
 - Bioset - Minster Auglaize Plt, Pop2,794
 - FKC Screw Press
- **ATAD**
 - Fuchs or Thermal Process Systems
 - Solar Drying
- **Composting**
 - CleanB-Pretreatment
- **Drying**
 - CleanB-Pretreatment




DISINFECTED & STABILIZED SEWAGE SLUDGE /BIOSOLIDS







Lime Use in Treating Sludge (Biosolids)

- **PSRP**
 - Lime slurry used to raise pH to 12 for 2 or more hours.
- **PFRP**
 - Quicklime (CaO) added to wet sludge cake to raise temperature to 70°C for 30 or more minutes.
 - Utilizes heat from exothermic reaction to raise temperature and high alkalinity to raise pH.






POST LIME TREATMENT OF SLUDGE





Untreated Sludge Calcium Oxide Lime treated biosolids supporting grass growth



Important Considerations with all Lime Processes


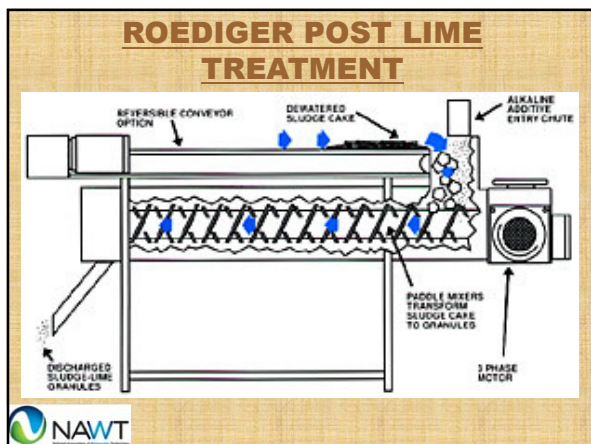
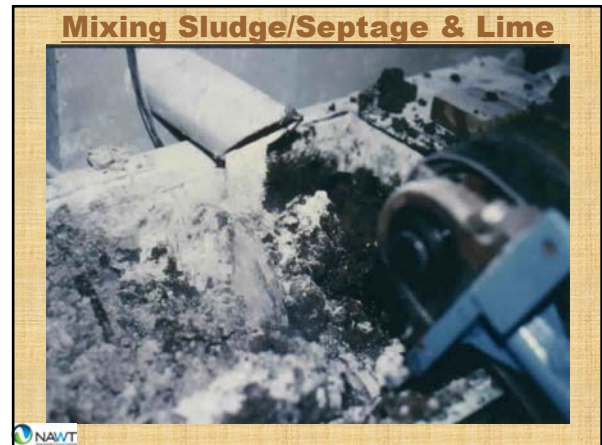
- Appear simple, inexpensive, easy option based on rules?
- Determination of Proper Lime Dose
- Proper pH determination
- Effects of Ammonia Gas on pH and Process
- Reactivity of Lime - Carbonated Hydrated Lime!!!
- Time/Temperature/pH
- Odor

Quicklime Reactivity

- Some Quicklime is Very (Violently) Reactive With Water
- Small particle Size is Important in Optimizing Exothermic Reaction
- Short Reaction Time Between Quicklime and Cake Biosolid Necessitates Optimum (Small) Particle Size to Maximize Heat Rise

Lime storage is another consideration:
 $Ca(OH)_2 + CO_2 \rightarrow CaCO_3 + H_2O$

Lime & Sludge Cake Mixing Study At DCWASA Blue Plains WWTP

Better mixing produced lower odors and less vectors
 Better mixing also released ammonia quickly, but dissipated quickly
 Poorer mixing produced less odors in beginning but odors persisted over longer time frames



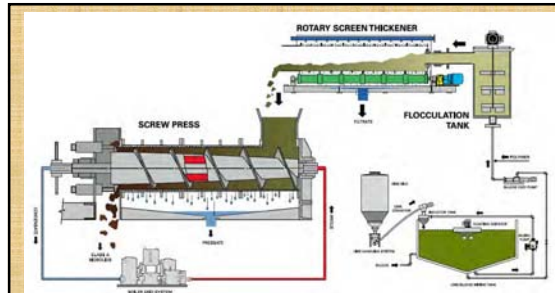
RDP Class A Pasteurization Process



From left to right, you see the sludge receiving hopper feeds the heated screw auger mixer. Lime is added to the mixer from the silo with a transverse auger. Blended material from the mixer is discharged into the pasteurizer where it is held at 70°C for 30 minutes and then discharged to a conveyor and placed in storage.



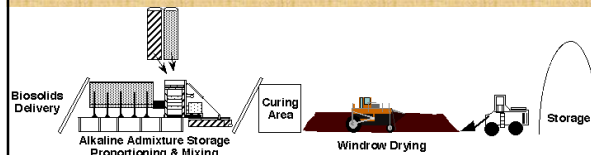
Class A Sludge/Septage Cake – Class A Biosolids



Simultaneous Dewatering & Pasteurization—FKC Class A Process



N-VIRO'S PROCESS



N-Viro Process Product



Fuchs ATAD

*Auto Thermal
Thermophilic Aerobic
Digestion*

Using Excess Heat - Example

- Bajo Ebro WWTP in Spain**
 - 1.5 mgd trickling filter plant producing 331 tons dry solids a year
 - Uses NILSA single reactor ATAD system
 - Loading: 32 g/l TS and 22 gr/l VS
 - HRT: 6-8 days
 - VSR: 28%
 - T of the process: 62°C
- Characteristics of the building to be heated**
 - Volume: 216 m³ (7628 ft³)
 - Room temperature: in between - 4°C and +10°C in fall
 - Time to heat the whole building from 9°C to 21°C is one-half hour.

Thermal Process Systems - ATAD

Solar Drying

A solar drying plant without supplemental heat would require two (2) chambers, each 42 ft wide by 216 ft long, or a total area of 18,190 ft². With 150 to 200 kW of waste heat availability you would only need 1 chamber of the same size as the solar only facility.



Solar Drying Bed

CleanB™ Process

- Total solids ≤ 2%
- Temperature ≥ 10 °C (50 °F)
- ORP > +100 mV
- Oxidant concentration 50 ppm or more as required to maintain ORP
- Oxidant contact time 10 minutes at > +100 mV

Benefits claimed for CleanB™ Process

- Reduce or eliminate need for digesters in some instances
- Create Class B biosolids in minutes
- Significantly reduce odors of residuals
- Reduce polymer consumption for dewatering
 - +30% reduction in polymer consumption






Aerated Static Pile Composting




Examples of using Thermal Dryers Washington State

Utility	Dryer Type/Brand	Product Amount (dt/year)	Price	Outlet	Annual Revenues
Camas	Belt/Andritz	350	NA	Parks, Golf courses planned	0
Alderwood	Belt/Kruger	300	Free	Compost facility	0
Selah	Indirect/Fenton	200	Free	Land application	0
Shelton	Belt/Andritz	Est. 500-750	Free	Give away to farmers	0






Example of Belt Dryer – Veolia Krueger BioCon






Example of Rotary Drum Dryer

Questions?